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(54) **PROCESS AND APPARATUS FOR PURIFYING MATERIAL OF BIOLOGICAL ORIGIN**

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203/72, 73, 80, 89; 159/5, 49

See application file for complete search history.

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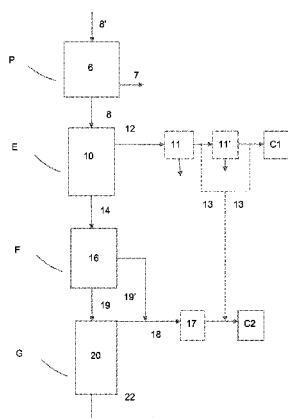
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**ABSTRACT**

The present invention relates to a process and an apparatus for purifying tall oil material for the production of biofuels and components thereof. The present invention relates further to hydroprocessing of the purified material to obtain biofuels and components thereof.

**15 Claims, 2 Drawing Sheets**



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**2400/26** (2013.01); **Y02E 50/13** (2013.01);  
**Y02T 50/678** (2013.01); **Y02W 30/74** (2015.05)
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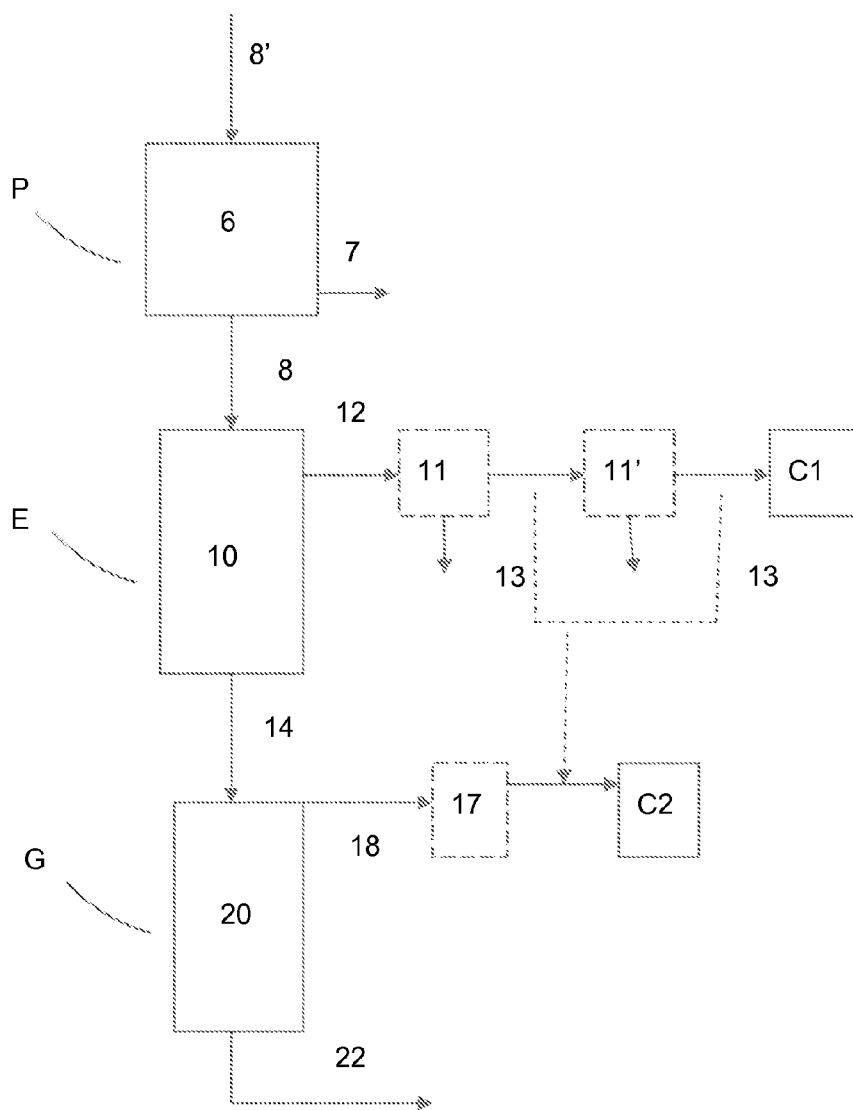


Fig. 1

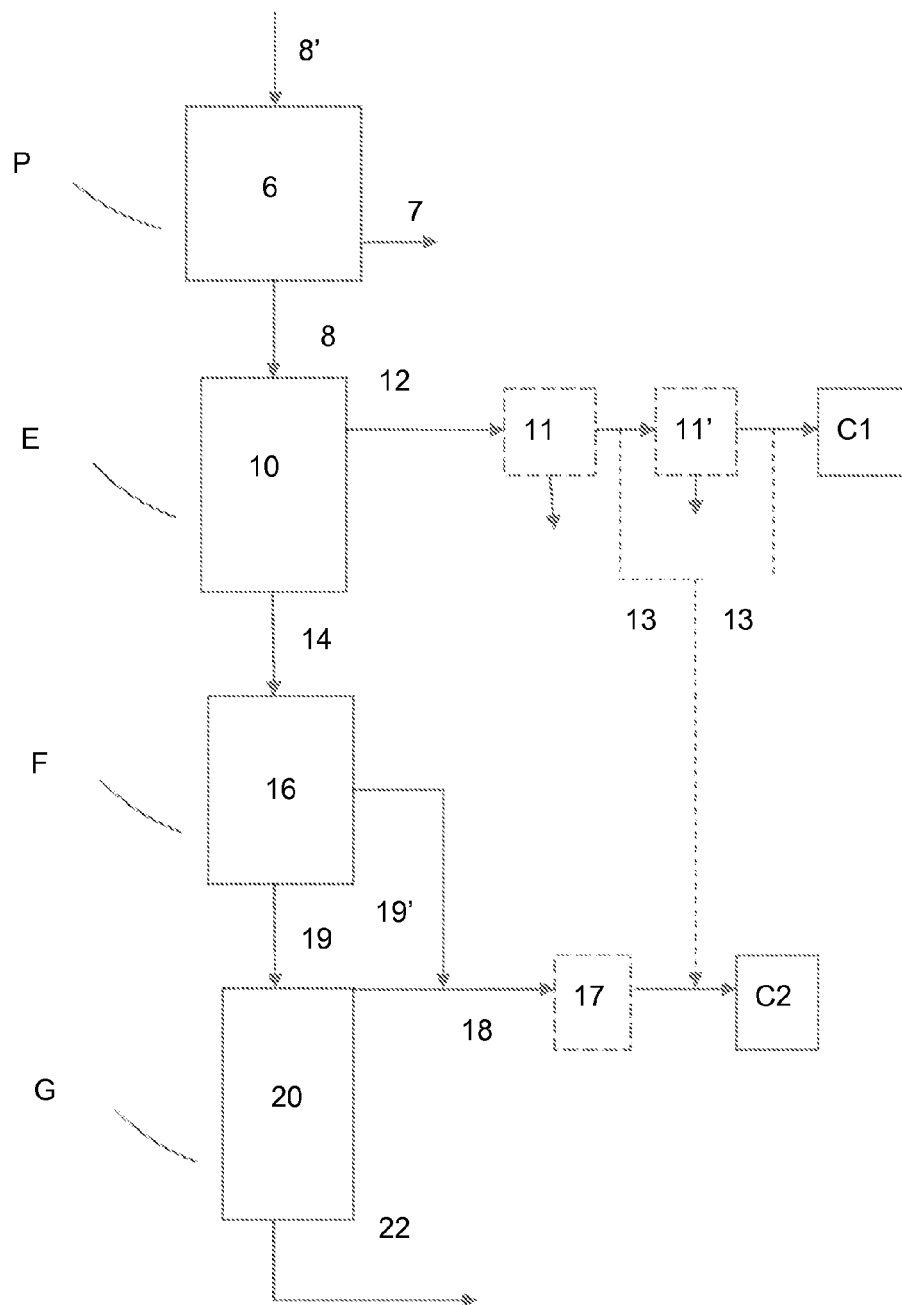


Fig. 2

## PROCESS AND APPARATUS FOR PURIFYING MATERIAL OF BIOLOGICAL ORIGIN

### CLAIM FOR PRIORITY

This application claims priority under 35 USC 371 to International Application No. PCT/FI2011/051037, filed on Nov. 25, 2011, which claims priority to Finnish Patent Application No. 20106252, filed Nov. 26, 2010, Finnish Patent Application No. 20115217, filed Mar. 3, 2011, and Finnish Patent Application No. 20115723, filed Jul. 6, 2011, each of which is hereby incorporated by reference in its entirety.

### FIELD OF THE INVENTION

The present invention relates to a process and an apparatus for purifying feed material of biological origin for the purposes of producing biofuels and components thereof. Especially the invention relates to a process and an apparatus for purifying tall oil material. The invention also relates to the use of the purified fractions recovered from the process for the production of biofuels and components thereof by hydroconversion processes.

### BACKGROUND OF THE INVENTION

Raw materials of biological origin are potential sources of various biofuels or biofuel components. These raw materials can be converted to biofuels by feeding the raw material through a catalytic reactor by contacting it simultaneously with gaseous hydrogen. The resulting product is drawn off from the reactor as a product stream which can be further fractionated for example by distillation to form biofuel/biofuel components.

There are however various problems related to production processes of biofuels from the raw materials of biological origin, such as poisoning and clogging of the catalyst material used in the production processes. There are impurities in the raw materials of biological origin, such as metals and solids that cause the inactivation of the catalyst material or cause coking on the catalyst and prevent it to function properly. In order to prevent the inactivation of the catalyst and to prolong its lifetime, the raw material can be purified and/or pretreated before feeding it to the hydrotreatment process. Purifying of the raw materials of biological origin to be suitable for feeding to a catalytic process is also challenging. Prior art describes various ways of doing this. However, these all have problems and the quality of the raw material is not always on a required level for the catalytic step to be able to function in the most efficient way.

One possibility of purifying and/or pretreating a raw material of biological origin, such as crude tall oil (CTO), which is to be fed to catalytic hydrotreatment processes, is ion-exchange with a cationic and/or anionic ion exchange resin.

Another possibility is to use methods such as adsorption on a suitable material or acid washing to remove alkaline metals and earth alkaline metals (Na, K, Ca). The adsorption material can be catalytically active or inactive. Yet another possibility is to use degumming for removing metals in the feed.

When the raw material of biological origin contains tall oil, depitching of the crude tall oil can also be used to remove impurities from the tall oil. Depitched tall oil is obtained by evaporating crude tall oil, for example by thinfilm evaporator. U.S. Pat. No. 5,705,722 describes converting unsaturated fatty acids, for example tall oil fatty acids to naphtha and cetane improvers for diesel fuels. However, this process has disadvantages, for example the yield of biofuel or biofuel

components, i.e. naphtha and cetane improvers, is poor. This is due to the fact that in depitching a huge amount of valuable raw material for hydrogenation is lost as residue, i.e. pitch. According to the document, the residue is used as such as fuel for boilers.

### BRIEF DESCRIPTION OF THE INVENTION

An object of the present invention is thus to provide a process and an apparatus for implementing the process so as to overcome the above problems. The objects of the invention are achieved by a process and an apparatus, which are characterized by what is stated in the independent claims. The preferred embodiments of the invention are disclosed in the dependent claims.

The present invention relates to a process for purifying tall oil material, comprising the following steps

(a) evaporating the tall oil material in a first evaporation step to produce a first fraction comprising light hydrocarbons and water and a second fraction comprising fatty acids, resin acids, neutral substances and residue components,

(b) evaporating said second fraction in at least one further evaporation step (G; F,G) to produce a third fraction comprising fatty acids, resin acids and light neutral substances, and a residue fraction, and

(c) recovering said first fraction, third fraction and residue fraction.

The present invention also relates to an apparatus for purifying tall oil material wherein the apparatus comprises

a first evaporator arranged to evaporate said tall oil material and to produce a first fraction comprising light hydrocarbons and water and a second fraction comprising fatty acids, resin acids, neutral substances and residue components,

at least one further evaporator arranged to evaporate said second fraction and to produce a third fraction comprising fatty acids, resin acids and light neutral substances and a residue fraction,

a first connection arranged to feed the second fraction to said at least one further evaporator, and optionally one or more further connections between said further evaporators.

In a preferred embodiment of the invention, said at least one further evaporation step is performed in one step, whereby the process as a whole comprises two evaporation steps. In another preferred embodiment of the invention, said at least one further evaporation step is performed in two steps, whereby the evaporation as a whole comprises three steps.

In a further preferred embodiment of the invention, the process further comprises a pretreatment step of storing the tall oil material in a storage tank before the first evaporation step.

The present invention also relates to the use of an apparatus comprising at least two sequentially arranged evaporators, for example three sequentially arranged evaporators, for purifying tall oil material.

Furthermore, the present invention relates to the use of the light hydrocarbons, fatty acids, resin acids and light neutral substances obtained in accordance with the process of the present invention for the production of biofuels and components thereof. Especially the invention relates to the use of the light hydrocarbons for the production of gasoline, naphtha, jet fuel, diesel and fuel gases and to the use of the fatty acids, resin acids and light neutral substances for the production of diesel, jet fuel, gasoline, naphtha and fuel gases.

The invention is based on the idea of purifying tall oil material to obtain purified hydrocarbon fractions. The purifi-

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cation in accordance with the present invention is performed by evaporation. The purified hydrocarbon fractions obtained in the process, after optional further purification, can be used as feedstock for the production of biofuels, such as biogasoline, biodiesel and/or components thereof. The purifying of the tall oil material in accordance with the present invention is performed by a multistep evaporation process, for example by a three-step process.

In the process of the present invention, the evaporation is accomplished in such a manner that the amount of residue from the evaporation is very small, typically ranging from 5% to 15%, preferably under 10% by weight from the feed. This is a great advantage over the prior art depitching processes, where the amount of the pitch residue from the evaporation may be as high as 20% to 35% by weight from the feed. In the present invention, the process conditions (temperature, pressure) are controlled in such a way that as much as possible of the neutral components of the tall oil material are withdrawn with the recovered fractions for further utilization, instead of being withdrawn with the residue as in the prior art tall oil depitching processes.

An advantage of the process and system of the invention comprising a multi-step evaporation is that when tall oil material is evaporated, the impurities, such as metals and solids are retained in the concentrate and the condensate retrieved from the evaporation is ready to be fed to the hydroprocessing reactor. Water and light components are first evaporated from the tall oil material, which makes further evaporation steps more efficient. Also the risk of carry-over of non-desired residual substances into the distillate fraction in the further evaporation steps is reduced in a controlled way. An advantage of such purifying with a multi-step evaporation is that the boiling takes place in a more controlled manner because low boiling light components, i.e. components having boiling point of 150-210° C., preferably 150-170° C., at a normal pressure, do not cause so much "carry over", i.e. migrating of the compounds having a boiling point range at the higher end of the above boiling point ranges as well as impurities to the vapour in the subsequent evaporation steps. The light components can be, if desired, returned back to the material of biological origin or refined further in another process or sold further as such.

A still further advantage of using three-step evaporation is that the evaporator in the second evaporation step can be a small and cheap evaporator that removes light components from the feed material. The following third evaporator can also be smaller and cheaper than the second evaporator in two-step evaporation. Consequently, a three-step evaporation unit can be cheaper than a two-step evaporation unit.

A still further advantage of the present invention compared to those known from the prior art is that the material purified according to the present invention is ready to be fed to hydroprocessing and the hydroprocessing is able to produce fuel components with excellent yield, because the pitch fraction is minimized.

A further advantage of the present invention is that the heavy components generated from the pitch can be avoided in the product fractions. A still further advantage of the present invention is that the yield of the purified material from the evaporation is as high as 65% to 95%, in a preferred embodiment from 80% to 95% and in a most preferred embodiment from 88% to 95%.

#### BRIEF DESCRIPTION OF THE DRAWINGS

In the following the invention will be described in greater detail by means of preferred embodiments with reference to the attached drawings, in which

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FIG. 1 shows a flowchart and an apparatus according to the present invention for the process for purifying tall oil material wherein the apparatus comprises two evaporators.

FIG. 2 shows a flowchart and an apparatus according to the present invention for the process for purifying tall oil material wherein the apparatus comprises three evaporators.

#### DETAILED DESCRIPTION OF THE INVENTION

Tall oil material in connection with the present invention refers to a byproduct of Kraft pulping of wood, especially coniferous wood. The tall oil material is a mixture of fatty acids, resin acids, neutral compounds and turpentine components originating from wood, especially coniferous wood. The turpentine components of tall oil are substantially composed of  $C_{10}H_{16}$  terpenes.

In one embodiment of the invention, the tall oil material is crude tall oil (CTO). CTO refers to the processed mixture of naturally-occurring compounds extracted from wood species like pine, spruce and aspen. It is obtained from the acidulation of crude tall oil soap from Kraft and sulphite pulping processes used in paper making. Crude tall oil (CTO) generally contains both saturated and unsaturated oxygen-containing organic compounds such as resin acids (mainly abietic acid and isomers thereof), fatty acids (mainly linoleic acid, oleic acid and linolenic acid), neutral substances, fatty alcohols, sterols and other alkyl hydrocarbon derivatives, as well as inorganic impurities (alkaline metal compounds, sulphur, silicon, phosphorus, calcium and iron compounds. CTO also covers soap oil.

In one embodiment of the invention, the tall oil material used for the feed or a part thereof may comprise purified CTO. Depitching, washing and/or distilling may be used for the purification of CTO.

In another embodiment of the invention, fatty acids or free fatty acids obtained from tall oil may be used as tall oil material, alone or as a mixture of other tall oil material.

In a further embodiment of the invention, soap oil may be used as the tall oil material for the feed. Also mixtures of soap oil and tall oil can be used as the tall oil material for the feed.

In connection with the present invention, the tall oil materials for the feed mixture are preferably selected from tall oil, crude tall oil (CTO), soap oil and mixtures thereof, for example.

The evaporation in connection with the present invention refers to any suitable separation method for separating two or more components from each other, such as gases from liquid, which separation method is based on utilising the differences in the vapour pressure of the components. Examples of such separation methods are evaporation, flashing and distillation. Preferably the evaporating is performed in an evaporator using thin film evaporation technology. In this embodiment of the invention, the evaporator can thus be selected from the group consisting of thin film evaporator, falling film evaporator, short path evaporator and plate molecular still and any other evaporator using thin film technology. The falling film evaporator refers to a falling film tube evaporator.

The evaporating in the process is performed with any commercially available suitable evaporators. Preferably the evaporating is performed in an evaporator selected from the group defined above. In an especially preferred embodiment of the invention, the evaporation is performed by evaporation using thin film evaporation. Suitable combinations for evaporators (in this order) in the evaporation unit are:

For two stage evaporation:  
TF+SP  
FF+TF

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TF+FF

TF+TF

For three stage evaporation:

TF+TF+SP

TF+PMS+SP

FF+TF+SP

FF+TF+TF

where

TF=thin film evaporator

FF=falling film tube evaporator

SP=short path evaporator

PMS=plate molecular still

Thus in one embodiment, the evaporation in a two-step evaporation is performed by using a thin film evaporator in the first evaporation step and a short path evaporator in the second evaporation step. In another embodiment, the two-step evaporation is performed by using a thin film evaporator in the first evaporation step and a falling film evaporator in the second evaporation step. Yet in another embodiment, the two-step evaporation is performed by using a thin film evaporator both in the first and second evaporation steps. In a preferred embodiment, the two-step evaporation is performed by using a falling film evaporator in the first evaporation step and a thin film evaporator in the second evaporation step.

In one embodiment of a three-step evaporation, the evaporation is performed by using a thin film evaporator in the first step, a plate molecular still in the second step and a short path evaporator in the third evaporation step. In another embodiment, the three-step evaporation is performed by using a thin film evaporator in the first step, a thin film evaporator in the second step and a short path evaporator in the third evaporation step. In another embodiment, the three-step evaporation is performed by using a falling film evaporator in the first step, a thin film evaporator in the second step and a short path evaporator in the third evaporation step. Yet in another embodiment, the three-step evaporation is performed by using a falling film evaporator in the first step, and a thin film evaporator in the second and third evaporation steps. The second evaporator in both two-step and three-step evaporation is most preferably a thin film evaporator.

In connection with the present invention, the impurities to be removed by the evaporation refer to water, solids, such as lignin, particulates, various inorganic compounds, metals, such as Na, Fe, P and Si, sulphur compounds, such as sulphates, for example  $\text{Na}_2\text{SO}_4$  and  $\text{H}_2\text{SO}_4$ , and organic compounds, such as carbohydrates. Many of these impurities (such as metals and sulphur compounds) are harmful in later catalytic hydroprocessing steps and are therefore not desirable in the feed to the hydroprocessing.

In the following, the process of the invention will be explained by referring to FIGS. 1 and 2, which are here to be contemplated as a flowchart of the process. FIG. 1 discloses a process comprising two-step evaporation. FIG. 2 discloses a process comprising three-step evaporation.

The evaporation in accordance with the present invention comprises a first evaporation step E and at least one further evaporation step shown by letter G or letters F and G. In accordance with the embodiment of FIG. 1, said at least one further evaporation step is performed in one step G, whereby the evaporation as a whole comprises two steps E, G. In accordance with FIG. 2, said at least one further evaporation step is performed in two steps F and G, whereby the evaporation as a whole comprises three steps E, F and G.

In the first evaporation step E, light hydrocarbons and water are evaporated off as distillate. Fatty acids, resin acids, neutral substances and residue components are remained as the evaporation concentrate.

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In said at least one further evaporation step (G; F,G), compounds comprising fatty acids, resin acids and light neutral substances are evaporated off as distillate. Residue components and heavy neutral substances are retained in the evaporation concentrate and are recovered as a first residue fraction (also named as a residue fraction in connection with the present invention).

In connection with the present invention, neutral substances of tall oil material refer to a mixture of components, such as esters of fatty acids, sterols, stanols, dimeric acids, resin and wax alcohols, hydrocarbons and sterol alcohols. Fatty acids and resin acids refer to those inherently present in tall oil material. Fatty acids mainly comprise linoleic acid, oleic acid and linolenic acid. Resin acids mainly comprise abietic acid and isomers thereof.

In connection with the present invention, the light hydrocarbons recovered from the first evaporation step E refer to hydrocarbons having a boiling point of up to  $250^\circ\text{C}$ . (NTP). These hydrocarbons mainly comprise terpenes, of which most is turpentine.

Said light neutral substances recovered in the distillate from said at least one further evaporation step (G; F,G) comprise  $\text{C}_{20}$ - $\text{C}_{27}$ -hydrocarbons, such as resin and wax alcohols, sterol alcohols and light sterols. The light neutral substances typically have a boiling point under  $500^\circ\text{C}$ . (NTP).

Said first residue fraction comprises heavy neutral substances and residue components, such as pitch and metals and other inorganic material. The first residue fraction typically contains components having a boiling point of over  $500^\circ\text{C}$ . (NTP).

Said heavy neutral substances recovered in the first residue fraction refer to hydrocarbons having at least 28 carbon atoms, such as sterols, stanols and dimeric acids, having a boiling point of over  $500^\circ\text{C}$ . (NTP).

The first evaporation step E is performed in a first evaporator 10. The evaporation is preferably performed at a temperature of 50 to  $250^\circ\text{C}$ . and at a pressure of 5 to 100 mbar, more preferably at a temperature of 120 to  $200^\circ\text{C}$ . and a pressure of 10 to 55 mbar. In the first evaporation step, water and light hydrocarbons are removed. The evaporation in the first evaporation step E is preferably performed by thin film evaporation.

According to the embodiment of FIG. 1, said at least one further evaporation step (second evaporation step in the embodiment of FIG. 1) is performed in one step G in a second evaporator 20. The second evaporation step is preferably effected at a temperature of 200 to  $450^\circ\text{C}$ . and a pressure of 0 to 50 mbar, more preferably at a temperature of 300 to  $390^\circ\text{C}$ . and a pressure of 0.01 to 15 mbar. Within this temperature and pressure range, the proportion of the pitch fraction (residue fraction) in this evaporation step is minimized. The evaporation in the second evaporation step G is preferably performed by short path evaporation.

According to the embodiment of FIG. 2, said at least one further evaporation step is performed in two steps F and G in two further evaporators 16 and 20. The first (F) of said two further evaporation steps (second evaporation step in the embodiment of FIG. 2) is preferably performed at a temperature of 180 to  $350^\circ\text{C}$ . and a pressure of 0.1 to 40 mbar, more preferably at a temperature of 200 to  $270^\circ\text{C}$ . and a pressure of 0.1 to 20 mbar. The second evaporation step F of the embodiment of FIG. 2 is preferably performed by plate molecular still evaporation or thin film evaporation. The third evaporation step G of the embodiment of FIG. 2 is preferably performed at a temperature of 200 to  $450^\circ\text{C}$ . and a pressure of 0 to 50 mbar, more preferably at a temperature of 300 to  $390^\circ\text{C}$ .

and a pressure of 0.01 to 10 mbar. The third evaporation step of the embodiment of FIG. 2 is preferably performed by short path evaporation.

The first evaporation step E in accordance with the present invention provides a first fraction comprising light hydrocarbons and water, which is withdrawn through the first product outlet 12. This fraction may be further treated by separating the water in water separation step 11, whereafter the light hydrocarbon fraction thus obtained may be subjected to one or more further purifications 11', for example by ion exchange. The light hydrocarbons of the first fraction may be then subjected to catalytic processes C1 for the production of biofuels and components thereof, such as gasoline, naphtha, jet fuel, diesel and fuel gases. The biofuels and components thereof produced from the light hydrocarbons of the first fraction refer to hydrocarbons having a boiling point in the range of 20 to 210° C., preferably 20 to 170° C. at a normal pressure.

The first evaporation step E also provides a second fraction comprising fatty acids, resin acids, neutral substances and residue components, such as pitch and metals. This second fraction is introduced into said at least one further evaporation step (G; F,G) for further purification through connection 14.

In accordance with the embodiment of FIG. 1, said second fraction comprising fatty acids, resin acids, neutral substances and residue components is introduced to the second evaporation step G through connection 14. The second evaporation step G in FIG. 1 is performed in a second evaporator 20. The second evaporation step G in FIG. 1 provides a third fraction comprising fatty acids, resin acids and light neutral components, which is withdrawn through a second product outlet 18. The second evaporation step G also provides a first residue fraction comprising residue components, such as pitch and metals. The first residue fraction is withdrawn through a first residue outlet 22.

In accordance with the embodiment of FIG. 2, said second fraction comprising fatty acids, resin acids, neutral substances and residue components is treated in two evaporation steps F and G, instead of only one step G. Said fraction is first introduced into a second evaporation step F through connection 14. The second evaporation step F in FIG. 2 is performed in a second evaporator 16. The liquid fraction from the second evaporator 16 is directed to a third evaporation step G through connection 19. The distillate fraction from the second evaporator step 16 is withdrawn through connection 19' and may be combined with the third fraction from the third evaporation step G. The third evaporation step G is performed in a third evaporator 20. The third evaporation step G in FIG. 2 provides a third fraction comprising fatty acids, resin acids and light neutral substances, which is withdrawn through a second product outlet 18. The third evaporation step G of FIG. 2 also provides a first residue fraction comprising residue components, such as pitch and metals. In the same way as in FIG. 1, the first residue fraction is withdrawn through the first residue outlet 22.

The third fraction withdrawn through the second product outlet 18 in the embodiments of FIGS. 1 and 2 may be then subjected to catalytic processes C2 for the production of biofuels and components thereof, such as diesel, jet fuel, gasoline, naphtha and fuel gases. The biofuels or components thereof produced from the third fraction refer to hydrocarbons having a boiling point in the range of 150 to 380° C. at a normal pressure.

In an embodiment of the invention, the process may further comprise a pretreatment step P of storing said tall oil material in a storage tank 6 before the first evaporation step E. In this embodiment of the invention, the tall oil material is intro-

duced to the first evaporation step E from a storage tank 6 through connection 8. In this embodiment of the invention, the tall oil material is kept in a storage tank for periods of hours to weeks before feeding to the first evaporation step E. This provides the advantage that non-desired components, such as water and solids separating from the tall oil by gravity and impurities such as metals and inorganic sulphur compounds dissolved or adsorbed/absorbed to them are separated from the tall oil material already in the storage tank and can be easily removed from the tall oil material for example by decantation through a second residue outlet 7 before feeding to the first evaporation step E.

In addition to selecting optimal evaporating process conditions in the evaporation steps E,F,G, the catalyst in the later hydroprocessing steps C1,C2 may be selected so that it is capable of transforming the heavy components in the purified material to biofuel components.

Between the last evaporation step G (the second evaporation step in the embodiment of FIG. 1 and the third evaporation step in the embodiment of FIG. 2) and hydroprocessing C2 there may be an additional purification step 17.

In one embodiment of the invention, the light hydrocarbons of the first fraction withdrawn through a connection 13 from the optional water removal step 11 or from one or optional further purification steps 11' may be combined with the third fraction comprising fatty acids, resin acids and light neutral compounds, which is withdrawn through the second product outlet 18 from the last evaporator 20. The fractions may be combined either before or after the additional purification step 17 of the third fraction.

The additional purification step 17 may be realised using for example a guard bed, i.e. a separate pretreatment/purification bed prior to the hydroprocessing C2. The additional purification 17 may also be realised by a purification bed or a section located in connection with the hydroprocessing reactor. The hydroprocessing optionally comprises one or more guard beds. The one or more guard beds can be arranged either to separate guard bed units and/or in the hydroprocessing reactor.

The guard bed has the task of acting against harmful substances in the feed. The guard bed is typically activated gamma aluminium oxide or some commercially available purifying catalyst. The guard bed material may be catalytically active or inactive. The guard bed or the guard bed units can retain both solid and solvated impurities of the tall oil material, such as silicon based anti-foaming agents of a tall oil process and harmful chemical elements. The guard bed and/or the guard bed units can be heated, unheated, pressurized or unpressurized, fed with hydrogen gas or without hydrogen gas. Preferably the guard bed and/or the guard bed units are heated and pressurized.

There are basically two types of guard beds, i.e. active and inactive guard beds. The active guard beds take part in the purification of the feed and changing the chemical composition of the feed and they can be placed either in separate guard bed units or inside the hydroprocessing reactor itself. The inactive guard beds merely take part in the purification of the feed. These guard beds comprise suitable passive or inert materials which do not significantly change the molecular structure of the feed components but are effective towards harmful substances and elements. The separate guard beds can be multiplied, whereby there is one or several guard beds in a stand-by mode in parallel or in series with the guard bed(s) in use.

After the purification by evaporating, the purified fractions are fed to the hydroprocessing. The fractions can be hydrotreated separately or in the same apparatus.



Consequently, the first and third fraction obtained from the process of the present invention and withdrawn through the first and second product outlets **12,18** may be further fed to hydroprocessing **C1, C2**, after an optional water removal step **11** and one or more optional further purification steps **11',17**. Hydroprocessing **C1,C2** comprises at least one catalyst to form a mixture of fuel components. The hydroprocessing can be done in one, two or more steps in one apparatus or in several apparatuses.

The light hydrocarbons of the first fraction withdrawn through the first product outlet **12** are hydroprocessed to obtain gasoline, naphtha, jet fuel, diesel and fuel gases.

The fatty acids, resin acids and light neutral substances withdrawn through the second product outlet **18** are hydroprocessed to obtain diesel, jet fuel, gasoline, naphtha and fuel gases.

The invention also relates to an apparatus for purifying tall oil material. The apparatus of the invention may be used for implementing the process of the invention. The apparatus of the invention will now be explained with reference to FIGS. **1** and **2**, which are here to be contemplated as referring to the elements of the apparatus.

The apparatus comprises

- a first evaporator **10** arranged to evaporate tall oil material and to produce a first fraction comprising light hydrocarbons and water and a second fraction comprising fatty acids, resin acids, neutral substances and residue components,
- at least one further evaporator (**20;16,20**) arranged to evaporate said second fraction and to produce a third fraction comprising fatty acids, resin acids and light neutral substances and a residue fraction,
- a first connection **14** arranged to feed the second fraction to said at least one further evaporator (**20;16,20**), and
- optionally one or more further connections **19** between said further evaporators **16,20**.

In accordance with the embodiment of FIG. **1**, said at least one further evaporator comprises one evaporator **20**. In this embodiment of the invention, the apparatus as a whole comprises two sequentially arranged evaporators **10** and **20**.

In accordance with the embodiment of FIG. **2**, said at least one further evaporator comprises two evaporators **16** and **20**. In this embodiment of the invention, the apparatus as a whole comprises three sequentially arranged evaporators **10, 16** and **20**.

The evaporators **10, 16, 20** mean here any suitable equipments for separating two or more components from each other, such as gases from liquid, which separator utilises the differences in the vapour pressure of the components. The separators and evaporators are described above in connection with the process of the invention. In the embodiments of FIGS. **1** and **2**, the first evaporator **10** is preferably a thin film evaporator or a falling film evaporator. In the embodiment of FIG. **1**, the second evaporator **20** is preferably a thin film evaporator. In the embodiment of FIG. **2**, the second evaporator **16** is preferably a plate molecular still or a thin film evaporator and the third evaporator **20** is preferably a short path evaporator. Most preferably the second evaporator is a thin film evaporator.

The apparatus further comprises a first product outlet **12** for recovering the fraction comprising light hydrocarbons and water from the first evaporator **10**, a second product outlet **18** for recovering the third fraction comprising fatty acids, resin acids and light neutral substances from said at least one further evaporator (**20;16,20**) and a first residue outlet **22** for recovering a first residue fraction containing pitch and metals from said at least one further evaporator (**20; 16,20**).

Referring to FIG. **2**, when said at least one further evaporator comprises two evaporators **16,20**, the second product outlet **18** and the first residue outlet **22** are connected to the last evaporator **20**.

In a typical embodiment of the invention, the apparatus further comprises one or more first feed inlets **8** arranged to feed the tall oil material to said first evaporator **10**.

The feed inlet/inlets **8** may be any suitable inlets for feeding the tall oil material to the system, such as pipe, hose, hole or any suitable connection.

According to an embodiment of the invention shown in FIGS. **1** and **2**, the apparatus may further comprise at least one storage tank **6** for the tall oil material located before the first evaporator **10** in the flow direction of the tall oil material. The storage tank in accordance with the present invention may be any suitable commercially available tank, vessel, container or such.

In this embodiment of the invention, the apparatus may further comprise a second residue outlet **7** for recovering a second residue fraction comprising water and inorganic material from the storage tank **6**.

In this embodiment of the invention, the apparatus may further comprise a second feed inlet **8'** for feeding the tall oil material to the storage tank **6**.

The apparatus of the invention may further comprise at least one catalytic hydroconversion unit **C1, C2** for converting the light hydrocarbons of the first fraction to one or more biofuels or components thereof selected from the group consisting of gasoline, naphtha, jet fuel, diesel and fuel gases and/or for converting the third fraction comprising fatty acids, resin acids and light neutral substances to one or more biofuels or components thereof selected from diesel, jet fuel, gasoline, naphtha and fuel gases.

Consequently, the light hydrocarbons of the first fraction recovered through the first product outlet **12** from the first evaporator **10** can be fed to a first catalytic hydroprocessing unit **C1** or to a second catalytic hydroprocessing unit **C2**.

The third fraction comprising fatty acids, resin acids and light neutral substances recovered through the second product outlet **18** from said at least one further evaporator **20** can be fed to a second catalytic hydroprocessing unit **C2**.

In the figures, the first and second catalytic hydroprocessing processes/units **C1,C2** are presented as separate units/processes. However, it is also possible to combine these units/processes and treat both recovered hydrocarbon fractions in one process having one or more process steps.

Referring to FIGS. **1** and **2**, the apparatus of the invention may also comprise a water separation unit **11** and one or more further purification units **11'** arranged before the first catalytic hydroprocessing unit **C1** and one or more further purification units **17** arranged before the second hydroprocessing unit **C2**. The apparatus may further comprise a connection **13** arranged after the water separation unit **11** or after said one or more further separation units **11'**, to feed the recovered light hydrocarbons of the first fraction to the third fraction withdrawn through connection **18**.

## EXAMPLES

In the following examples 1 and 2, the impurities in the material of biological origin were removed by two different evaporation units. In Example 1, the evaporation unit comprised of two evaporators and in Example 2 the evaporation unit comprised of three evaporators. The material of biological origin was crude tall oil.

### Example 1

Crude tall oil (CTO) was fed from storage at a temperature of 60° C. to an evaporation unit containing a thin film evapo-

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rator and a short path evaporator. The feed rate of the crude tall oil to the evaporation unit was between 30-80 kg/h. The temperature of the first evaporation step was 137° C. and the pressure was 18 mbar. A first fraction comprising water and turpentine was removed from the feed of crude tall oil.

The first evaporation step was performed on a thin film evaporator. In the first evaporator, all together 3% of the original amount of crude tall oil was evaporated, of which 2% was turpentine and other light hydrocarbon compounds and 1% was water. 97% of the amount of the original feed of crude tall oil was recovered as condensate, i.e. second fraction, from the first evaporator and fed further to a second evaporator. The second evaporation step was performed on a short path evaporator at 315° C. and 0.3 mbar. 5% of the amount of the original feed was removed from the second evaporation step as a residue fraction comprising pitch. Distillate, third fraction, was recovered from the second evaporating step and the amount of it was 92% of the amount of the original feed of crude tall oil. The residue fraction removed from the second evaporator contained 1600 ppm metals in total consisting mainly of Na, Fe, P and 10 to 20 other metals, and in addition to metals also  $\text{SO}_4^{2-}$ , in the form of  $\text{Na}_2\text{SO}_4$  and lignin.

## Example 2

Crude tall oil (CTO) with a metal content of 72 ppm was fed from storage at a temperature of 60° C. to an evaporation unit containing a thin film evaporator, a plate molecular still and a short path evaporator. The feed rate of the crude tall oil to the evaporation unit was between 30-80 kg/h. The temperature of the first evaporation step was 137° C. and the pressure was 18 mbar. A first fraction comprising water and turpentine was removed from the feed of crude tall oil.

The first evaporation step was performed on a thin film evaporator. In the first evaporator, all together 3% of the original amount of crude tall oil was evaporated, of which 2% was turpentine and other light hydrocarbon compounds and 1% was water. 97% of the amount of the original feed of crude tall oil was recovered as condensate, i.e. second fraction from the first evaporator and fed further to a second evaporator. The second evaporation step was performed on a plate molecular still at 220° C. and 1 mbar. 50% of the amount of the original feed of crude tall oil was removed from the second evaporation step as a liquid fraction. Distillate fraction was recovered from the second evaporating step and the amount of it was 47% of the amount of the original feed of crude tall oil. The liquid fraction from the second evaporation step was fed to the third evaporation step. The third evaporation step was performed on a short path evaporator at 330° C. and 0.1 mbar. The amount of the residue fraction removed from the third evaporator was 5.5% from the original feed and it contained 1550 ppm metals in total, consisting mainly of Na, Fe, P and 10 to 20 other metals, and in addition to metals also  $\text{SO}_4^{2-}$ , in the form of  $\text{Na}_2\text{SO}_4$  and lignin. Distillate, third fraction, was also recovered from the second evaporating step. Distillates from evaporation stages 2 and 3 were collected and mixed together. The purified CTO had a 5 ppm metal content.

From the examples above it is obvious that using a multi-stage evaporation according to the invention for purifying CTO is a very efficient method for removing impurities from it. It is also obvious that by using the process according to the invention, light neutral components can be separated to be processed to raw materials for valuable transportation fuel products and the amount of the residue fraction, pitch, is minimized.

It will be obvious to a person skilled in the art that, as the technology advances, the inventive concept can be imple-

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mented in various ways. The invention and its embodiments are not limited to the examples described above but may vary within the scope of the claims.

The invention claimed is:

1. A process for purifying tall oil material, comprising the following steps

(a) evaporating the tall oil material in a first evaporation step (E) to produce a first fraction comprising hydrocarbons having a boiling point of up to 250° C. at normal pressure and water and a second fraction comprising fatty acids, resin acids, neutral substances and residue components,

(b) evaporating said second fraction in at least one further evaporation step (F,G) to produce a third fraction comprising fatty acids, resin acids and neutral substances having a boiling point under 500° C. at normal pressure, and a residue fraction, wherein said at least one further evaporation step (F,G) is performed in two steps (F,G), whereby the first (F) of said two further evaporation steps is performed at a temperature of 180 to 350° C. and at a pressure of 0.1 to 40 mbar and the second (G) of said two further evaporation steps is performed at a temperature of 200 to 450° C. and at a pressure of 0 to 50 mbar, and

(c) recovering said first fraction, third fraction and residue fraction.

2. The process according to claim 1, wherein the evaporation in the first evaporation step (E) and said further evaporation steps (F,G) is performed by evaporation using thin film evaporation technology.

3. The process according claim 2, wherein the evaporation in the first evaporation step (E) and in the further evaporating steps is performed by thin film evaporation, falling film evaporation, short path evaporation or plate molecular still evaporation.

4. The process according to claim 1, wherein the tall oil material is a by-product of Kraft pulping of wood.

5. The process according to claim 1, wherein the tall oil material is selected from the group consisting of tall oil, crude tall oil (CTO), soap oil and mixtures thereof.

6. The process according to claim 1, wherein the neutral substances having a boiling point under 500° C. at normal pressure of said third fraction comprise  $\text{C}_{20}$ - $\text{C}_{27}$ -hydrocarbons.

7. The process according to claim 1, wherein said residue fraction comprises heavy neutral substances and residue components.

8. The process according to claim 7, wherein said heavy neutral substances comprise hydrocarbons having at least 28 carbon atoms, having a boiling point of over 500° C. at normal pressure.

9. The process according to claim 1, wherein the process comprises a further step (11) of separating water from the first fraction, followed by one or more optional further purification steps (11').

10. The process according to claim 1, wherein the process further comprises one or more purification steps (17) for the third fraction.

11. The process according to claim 1, wherein the process further comprises one or more hydroprocessing steps (C1, C2) to convert the recovered first and third fraction to bio fuels or components thereof, after an optional water separation step (11) and one or more optional further purification steps (11', 17).

12. The process according to claim 11, wherein the process further comprises one or more of the hydroprocessing steps (C1) of converting the first fraction to one or more biofuels or

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components thereof selected from the group consisting of gasoline, naphtha, jet fuel, diesel and fuel gases.

**13.** The process according to claim **11**, wherein the process further comprises one or more of the hydroprocessing steps (C2) of converting the third fraction to one or more biofuels or components thereof selected from the group consisting of diesel, jet fuel, gasoline, naphtha and fuel gases. 5

**14.** The process according to claim **4**, wherein the wood is coniferous wood.

**15.** The process according to claim **1**, wherein the evaporation step (E) is performed at a temperature of 50 to 250° C. and at a pressure of 5 to 100 mbar. 10

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